

PATENT SPECIFICATION

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COMPLETE SPECIFICATION

Improvements in and relating to the Decomposition of Titanium Salt Solutions by Hydrolytic Precipitation

We, TITAN COMPANY INC., a Corporation organised under the laws of the State of Delaware, United States of America, of Wilmington, Delaware,
5 United States of America, and having an
office address at 111, Broadway, City,
County and State of New York, United States of America, do hereby declare the nature of this invention and in what 10 manner the same is to be performed, to be particularly described and ascertained in and by the following statement:-

The invention relates to the production of titanium dioxide pigments by the 15 hydrolytic precipitation of titanium salt solutions and the calcination of the pre-

cipitate. In British Patent Specification No. 481,892 it is explained that titanium di-481,892 it is explained that intamium uroxide obtained by the calcination of the
precipitate of a titanium salt solution
may exist as the anatase modification
(refractive index 2.55) or the rutile modification (refractive index 2.71). Further
that the anatase modification may be
obtained from titanium sulphate solutions and the rutile modification from titanium chloride solutions. In view of the higher refractive index of the rutile 30 modification it would be desirable to employ titanium chloride solutions, but at the present day commercial production is confined almost entirely to the prepara-tion of the anatase modification from sul-35 phuric acid solutions, owing to the diffi-culty met on a commercial scale in obtaining precipitated particles of suitable form for pigment purposes from the titanium chloride solutions, the precipi-40 tate normally being in a very fine state of division and in consequence difficult to filter and impossible to wash free from impurities contained in the mother 45 been carried out on the preparation of titanium dioxide pigments from titanium salt solutions, and particular attention has been paid to the possibilities of ob-taining products of suitable form from 50 titanium chloride solutions. The result of the investigations has been a number

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of suggestions, some of which have been adopted in practice, either to add to the solution materials which will assist the hydrolysis and influence the nature of the precipitate, or to effect the hydrolysis in the presence of suspended insoluble materials which influence the nature of the precipitate. British Specification No. 308,725 describes the hydrolytic precipitation of titanium compounds from mineral acid titaniferous solutions by adding the solution to a hot aqueous bath and in order to prevent aggregation an organic acid with or without phosphoric acid is dissolved in the hydrolysis liquor. No specific limits are given for the quantity of organic acid but a fairly large proportion is contemplated as the amount is compared with that required for a double decomposition reaction with the titanium content. As is described in Specification No. 481,892, whilst the acids have a dispersing action when used in the proportions described in No. 308,725, a very small quantity in a titanium chloride solution has the surprising effect of acting as an aggregation agent. British Specification No. 433,960 describes a process in which hydrolysis of a titanium salt solution is effected in the presence of a small amount of a finely dispersed titanium salt which is diffi-cultly soluble in dilute mineral acids. Examples of such salts are titanium phosphate, titanium potassium sulphate and titanium potassium fluoride. These salts provide "nuclei" for facilitating the precipitation.

The process described and claimed in Specification No. 481,892 already referred to above is a process for the production of titanium dioxide having the rutile crysalline structure comprising hydrolysing an aqueous solution of titanium tetrachloride and calcining the precipitate wherein the hydrolytic precipitation is effected in the presence of negative divalent ions derived from a substance added to the solution in a proportion not 100 exceeding 0.1 mol. to each mol. titanium

reckoned as TiO2 present in the hydrolysis

solution, and wherein the hydrolytic precipitation is effected in the absence of any added insoluble material suspended in the solution. It has now been found that the same desirable results, namely, the production of titanium dioxide having the rutile crystalline structure in a suitable form as regards particle size, can be obtained by 10 the hydrolytic precipitation of aqueous solution of titanium tetrachloride in the presence of other negative polyvalent ions, that is ions having a valency of three or more. Furthermore, it has 15 been found that the same desirable results may be obtained by the hydrolytic preciptation of aqueous solutions of titanium fluorides and complex titanium fluorine compounds in the presence of 20 negative ions having a valency of two or more. In both cases the substance from which the negative polyvalent ions are derived is added in very small quantities, namely, not more than 0.01 mol of the 25 substance to each mol of titanium reckoned as TiO2 present in the solution. The present invention accordingly comprises a process for the production of titanium dioxide having the rutile 30 crystalline structure comprising hydrolytically precipitating an aqueous solu-tion of titanium tetrachloride, of titanium fluoride or of a complex titanium fluorine compound and calcin-35 ing the precipitate wherein, in order to obtain an easily filtrable hydrated titanium compound the hydrolytic precipitation is effected in the presence of a small amount of a negative polyvalent 40 ion which, with a titanium fluoride or complex titanium fluorine solution, has a valency of two or more and, with a titanium tetrachloride solution, has a valency of three or more, the substance 45 from which the negative polyvalent ion is derived being present in an amount not greater than 0.01 mol of the substance to each mol of titanium reckoned as TiO₂.

The negative polyvalent ions employed may be ions of inorganic acids and of ionisable organic acids. For example divalent ions, the use of which is only claimed in the present application in con-55 nection with solutions of titanium fluoride and complex titanium fluorine compounds since the use of such ions in conjunction with titanium tetrachloride solutions is claimed in Specification No. 60 481,892, may be obtained by the addition to the hydrolysis solution of sulphuric, arsenic, carbonic, oxalic or tartaric acid or one of their alkali metal salts. valent ions, the use of which is claimed 65 in the present application both in con-

nection with tetrachloride, titanium fluorides and complex titanium fluorine compounds, may for example be obtained by the addition of phosphoric or citric acid or a soluble alkali metal phosphate or citrate. More specific examples of salts which may be employed to give the negative ions are sodium sulphate, ammonium oxalate, lithium carbonate, sodium arsenate, sodium citrate and potassium tartrate. A solution containing the ion may be added to the titanium solution, or alternatively the titanium solution may be added to the solution containing the ion. Conveniently the acid or salt is dissolved in a large volume of water, the temperature is then raised and the titanium solution added. Only a small amount of the polyvalent

ion is required, to obtain the desired result, and as the polyvalent negative ions have a tendency to associate themselves, for example by adsorption, with the particles of hydrated titanium dioxide and they are not removed by washing, this effect being particularly noticeable with the sulphate and phosphate ions, the amount of polyvalent ion employed must not be so great as to contaminate undesirably the hydrated titanium dioxide.

The titanium solution is preferably relatively concentrated containing approximately 15% of titanium calculated as TiO2, and it should be substantially free from impurities. Such solutions give 100 optimum results, but no particular concentration of titanium nor any particular condition of purity of the solution is essential for the successful carrying out

of the process of the invention.

The term "titanium fluorides and complex titanium fluorine compounds" is used broadly in this specification and in the claims to include not only titanium tetrafluoride but also complex 110 fluorides of titanium, for example amino titanium tetrafluorides, TiF4. x NH2, and those compounds of titanium which are sometimes regarded as the double fluorides of titanium and other elements or 115 radicals, for example TiF4. × NH4F, as well as combinations of such compounds for example $TiF_4 imes NH_3 imes NH_4F$.

The desirable effects obtained by using the polyvalent ions in accordance with 120 the present invention are obtained regardless of the exact method adopted for hydrolytically precipitating the hydrated titanium dioxide from the titanium solu-tion; for example, the hydrated titanium 125 dioxide may be hydrolytically precipitated in the well known manner by raising the temperature of the solution to, or approaching, the boiling point which step may or may not be accompanied by 180

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a dilution of the titanium solution.

The hydrolytic precipitation is preferably carried out under such conditions as to give relatively rapid precipitation. It 5 is found that the presence of the polyvalent negative ions has the effect of preventing the precipitated particles assuming an extremely fine form so that the particles obtained are of a suitable size 10 for pigment purposes. The precipitate is thus readily filterable and easily washed. Furthermore, the precipitate when calcined gives a product having the rutile crystalline structure and having a re-15 markably high hiding power and tinting strength.

The process of the present invention is illustrated by the following specific

Examples:-

EXAMPLE 1.

20 Titanium tetrachloride is dissolved in cold water to give a clear aqueous solution of titanium containing about 15 per cen, of titanium reckoned as TiO₂. All 25 the iron present is reduced to the ferrous condition in order to prevent the hydrolysis which ferric salts readily undergo. In order to ensure the absence of ferrio iron throughout the precipitation it is 30 preferable to reduce the solution to a content of two to three grams per litre of trivalent titanium reckoned as TiO₂. 1000 kilos of the chloride solution containing 15 per cent. titanium reckoned as 35 TiO₂ are added to 7000 litres of boiling water containing two kilos of citric acid, during about one hour. When the addi-tion has been completed about 95 per cent. of the titanium will have been pre-40 cipitated as hydrated titanium dioxide; the latter is in a coagulated form such that it settles well and may be readily filtered and washed. After filtration and washing the precipitate is calcined at a 45 temperature of from 700 to 1000° C.

EXAMPLE 2. Ilmenite is furnaced with ammonium fluoride and the vapours of diamino tetrafluoride TiF₄.2NH₃, are collected. 50 tetrafluoride compound is dissolved in water containing sodium sulphate, the necessary quantities being used to obtain a solution containing about ten per cent. by weight of titanium reckoned as TiO₂ 55 and 0.05 per cent. by weight of sulphate

The solution is then boiled to radical. precipitate hydrated titanium dioxide in a filterable condition. The precipitate is washed and calcined.

Having now particularly described and 60 ascertained the nature of our said invention and in what manner the same is to be performed, we declare that what we claim is:-

1. A process for the production of 65 titanium dioxide having the rutile crystalline structure comprising hydrolytically precipitating an aqueous solu-tion of titanium tetrachloride, of titanium fluoride or of a complex 70 titanium fluorine compound and calcining the precipitate wherein in order to filtrableobtain an easily hydrated titanium compound, the hydrolytic precipitation is effected in the presence of a 75 small amount of a negative polyvalent ion which, with a titanium fluoride or complex titanium fluorine solution, has a valency of two or more and, with a titanium tetrachloride solution, has a 80 valency of three or more, the substance from which the negative polyvalent ion is derived being present in an amount not greater than 0.01 mol of the substance to each mol of titanium reckoned as 85 TiO₂.

2. A process as claimed in Claim 1 wherein the polyvalent ion is obtained by the addition of phosphoric or citric acid or an akali metal phosphate or citrate to 90

the solution.

3. A process as claimed in Claim 1 wherein a fluoride solution is employed and the polyvalent ion is obtained by adding oxalic, tartaric, sulphuric, arsenic or 95 carbonic acid or one of their alkali metal salts to the solution.

4. A process as claimed in any one of the preceding Claims carried out substantially in the manner hereinbefore hereinbefore 100

described.

5. Calcined titanium dioxide having the rutile structure when obtained by the process claimed in any one of the preceding claims.

Dated this 5th day of November, 1937. BOULT, WADE & TENNANT, 111 & 112, Hatton Garden, London, E.C.1,

Chartered Patent Agents.